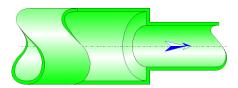


Sudden Contraction Sharp Circular Cross-Section (MILLER)



Model description:

This model of component calculates the minor head loss (pressure drop) generated by the flow in a sudden contraction sharp.

The head loss by friction in the inlet and outlet piping is not taken into account in this component.

Model formulation:

Major cross-sectional area (m²):

$$A_1 = \pi \cdot \frac{D_1^2}{4}$$

Minor cross-sectional area (m2):

$$A_2 = \pi \cdot \frac{D_2^2}{4}$$

Mean velocity in major diameter (m/s):

$$U_1 = \frac{Q}{A_1}$$

Mean velocity in minor diameter (m/s):

$$U_2 = \frac{Q}{A_2}$$

Mass flow rate (kg/s):

$$G = Q \cdot \rho$$

Reynolds number in major diameter:

$$Re_1 = \frac{U_1 \cdot D_1}{v}$$

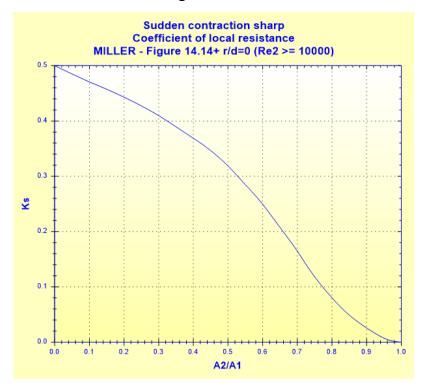
Reynolds number in minor diameter:

$$Re_2 = \frac{U_2 \cdot D_2}{v}$$

Local resistance coefficient :

$$K_{s} = f\left(\frac{A_{2}}{A_{1}}\right)$$

([1] figure 14.14+ r/d=0)



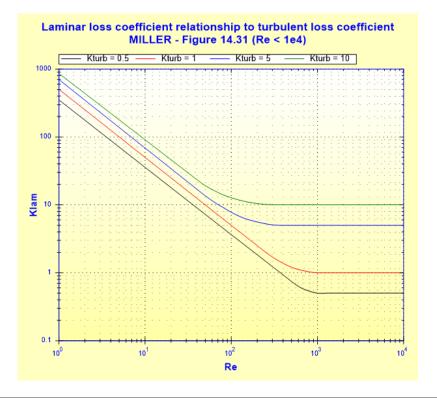
■ $Re_2 < 10^4$

$$K_{lam} = f(K_{turb}, Re_2)$$

([1] figure 14.31)

where:

 K_{turb} is the local resistance coefficient in turbulent regime (K_s for $Re_2 = 10^4$ - figure 14.14+ r/d=0)



Reynolds Number Correction ($Re_2 < 10^4$):

$$C_{\text{Re}} = \frac{K_{lam}}{K_{turb}}$$

Total pressure loss coefficient (based on mean velocity in minor diameter):

■ turbulent flow (Re₂ \geq 10⁴):

$$K = K_s$$

■ laminar flow (Re₂ < 10^4):

$$K = K_{lam}$$

Total pressure loss (Pa):

$$\Delta P = K \cdot \frac{\rho \cdot U_2^2}{2}$$

Total head loss of fluid (m):

$$\Delta H = K \cdot \frac{{U_2}^2}{2 \cdot g}$$

Hydraulic power loss (W):

$$Wh = \Delta P \cdot Q$$

Symbols, Definitions, SI Units:

 D_1 Major diameter (m)

D₂ Minor diameter (m)

A₁ Major cross-sectional area (m²)

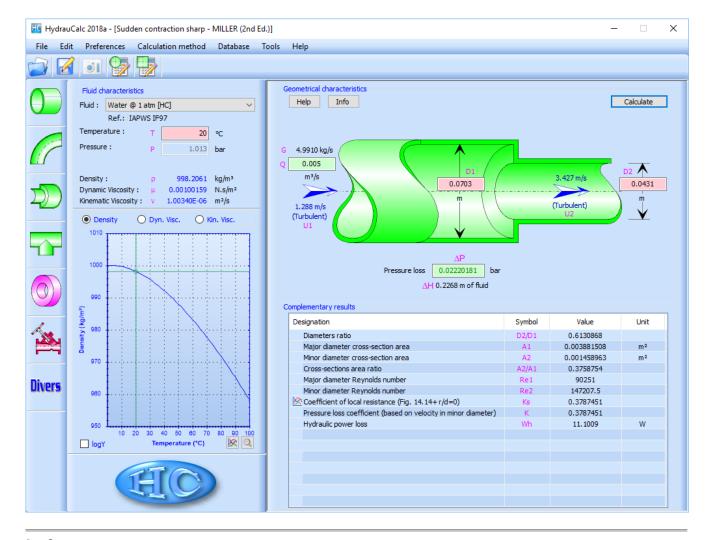
 A_2 Minor cross-sectional area (m²) Volume flow rate (m³/s) Q G Mass flow rate (kg/s) Mean velocity in major diameter (m/s) U₁ Mean velocity in minor diameter (m/s) U₂ Reynolds number in major diameter () Re₁ Reynolds number in minor diameter () Re2 Ks Local resistance coefficient for $Re_2 \ge 10^4$ () Local resistance coefficient for $Re_2 = 10^4$ () K_{turb} Local resistance coefficient for $Re_2 < 10^4$ () Klam Reynolds number correction for $Re_2 < 10^4$ () C_{Re} Κ Total pressure loss coefficient (based on mean velocity in minor diameter) () Total pressure loss (Pa) ΔP ΔH Total head loss of fluid (m) Wh Hydraulic power loss (W) Fluid density (kg/m³) ρ Fluid kinematic viscosity (m²/s) ν Gravitational acceleration (m/s^2) g

Validity range:

any flow regime: laminar and turbulent

note: for Reynolds number " Re_2 " lower than 10^4 , and coefficients " K_{turb} " lower than 0.5 or greater than 10, the laminar pressure loss coefficient is extrapolated

Example of application:



References:

[1] Internal Flow System, Second Edition, D.S. Miller

HydrauCalc Edition: February 2018

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