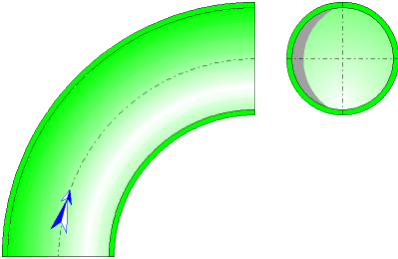




Smooth Bend Circular Cross-Section (IDELCHIK)



Model description:

This model of component calculates the head loss (pressure drop) of a bend smoothly curved whose cross-section is circular and constant. In addition, the flow is assumed fully developed and stabilized à the entrance bend.

Model formulation:

Hydraulic diameter (m):

$$D_h = D_0$$

Cross-section area (m²):

$$F_0 = \pi \cdot \frac{D_0^2}{4}$$

Length measured along the axis (m):

$$l = 2 \cdot \pi \cdot R_0 \cdot \frac{\delta}{360}$$

Mean velocity (m/s):

$$w_0 = \frac{Q}{F_0}$$

Mass flow rate (kg/s):

$$G = Q \cdot \rho$$

Fluid volume (m³):

$$V = F_0 \cdot l$$

Fluid mass (kg):

$$M = V \cdot \rho$$

Reynolds number:

$$Re = \frac{w_0 \cdot D_h}{\nu}$$

Relative roughness:

$$\bar{\Delta} = \frac{\Delta}{D_0}$$

■ Case of relative radius of curvature lower than 3 ($R_0/D_0 < 3$) ([1] diagram 6.1)

Coefficient of effect of the roughness:

$$k_{\Delta} = f\left(\frac{R_0}{D_0}, Re, \bar{\Delta}\right) \quad ([1] \text{ diagram 6.1})$$

● $0.50 \leq R_0/D_0 \leq 0.55$

$\bar{\Delta}$	Re	
	$3 \cdot 10^3 - 4 \cdot 10^4$	$> 4 \cdot 10^4$
0	1.0	1.0
0 - 0.001	1.0	$1 + 0.5 \cdot 10^{-3} \cdot \bar{\Delta}$
> 0.001	1.0	1.5

● $R_0/D_0 > 0.55$

$\bar{\Delta}$	Re		
	$3 \cdot 10^3 - 4 \cdot 10^4$	$> 4 \cdot 10^4 - 2 \cdot 10^5$	$> 2 \cdot 10^5$
0	1.0	1.0	1.0
0 - 0.001	1.0	$\lambda_{\Delta} / \lambda_{sm}$	$1 + 10^{-3} \cdot \bar{\Delta}$
> 0.001	1.0	2.0	2.0

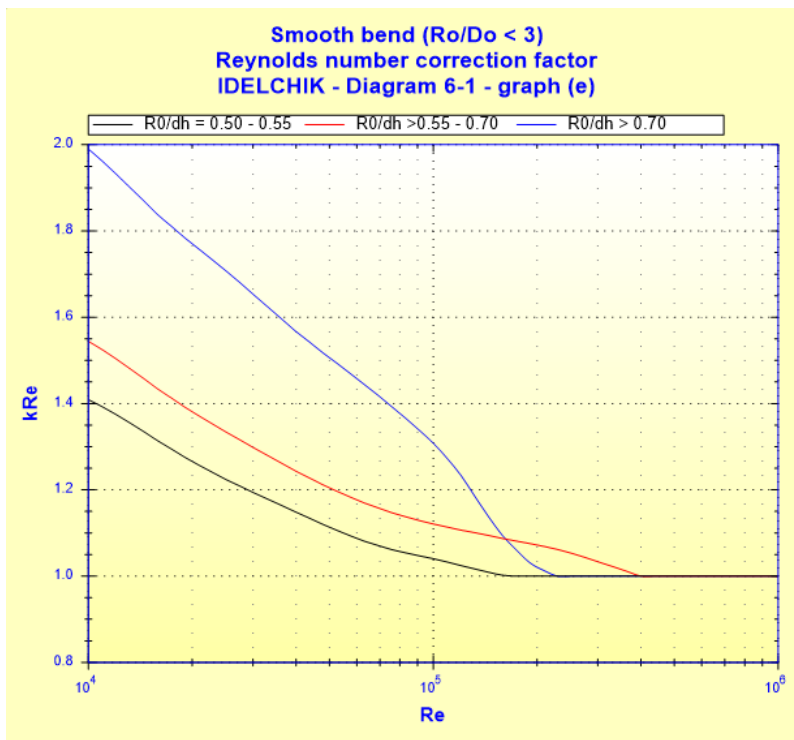
with:

λ_{sm} : Darcy friction factor for hydraulically smooth pipe ($\bar{\Delta} = 0$) at Re

λ_{Δ} : Darcy friction factor for rough pipe ($\bar{\Delta} = \Delta/D_h$) at Re

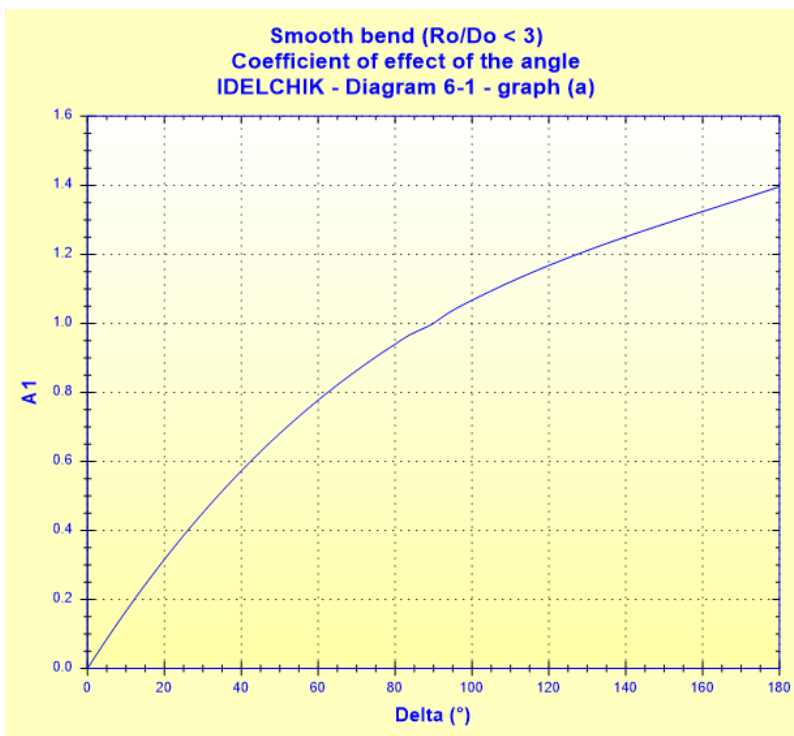
Coefficient of effect of the Reynolds number ($Re \geq 10^4$):

$$k_{Re} = f\left(Re, \frac{R_0}{D_h}\right) \quad ([1] \text{ diagram 6.1})$$



Coefficient of effect of the angle:

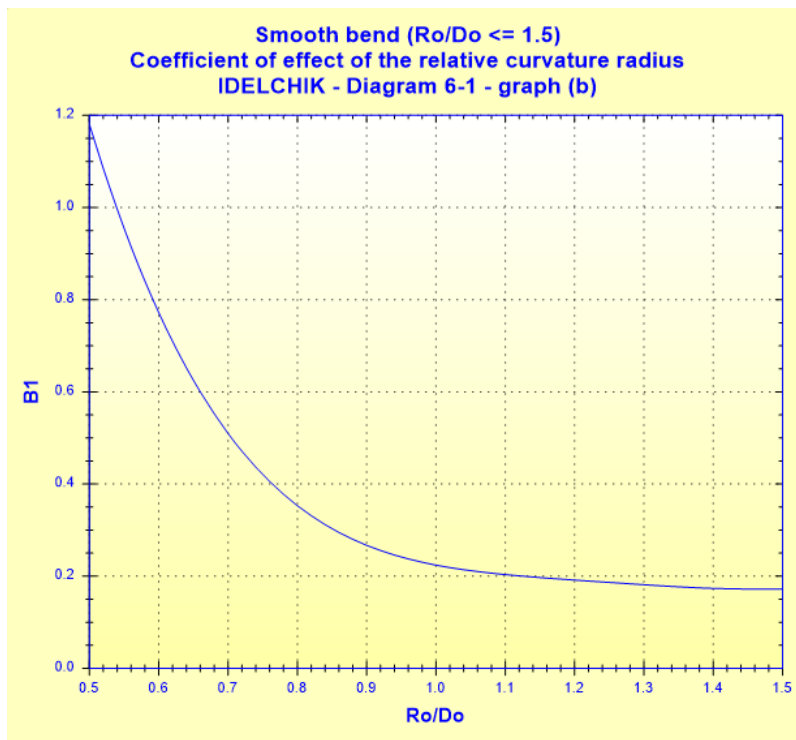
$$A1 = f(\delta) \quad ([1] \text{ diagram 6.1})$$



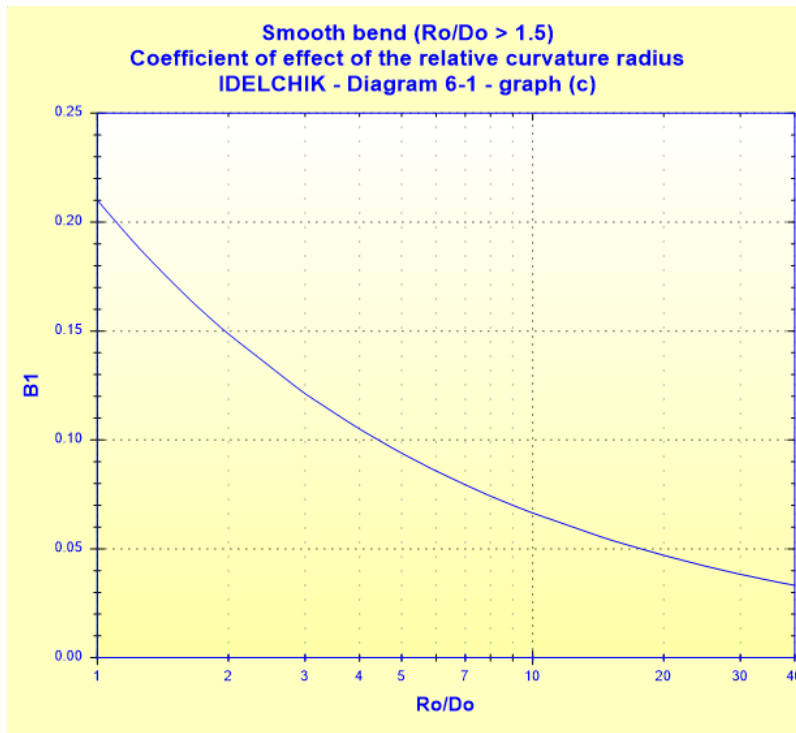
Coefficient of effect of the relative curvature radius:

$$B1 = f\left(\frac{R_0}{D_h}\right) \quad ([1] \text{ diagram 6.1})$$

- $0.5 \leq R_0/D_0 \leq 1.5$



- $R_0/D_0 > 1.5$



Coefficient of effect of the relative elongation of the cross section:

$$\boxed{C_1 = 1} \quad ([1] \text{ diagram 6.1})$$

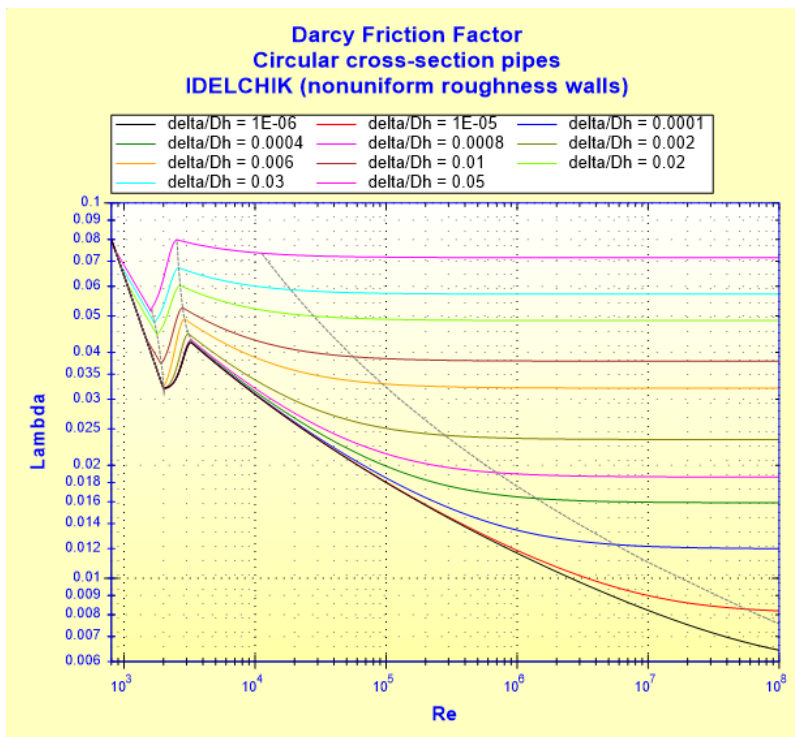
Coefficient of local resistance:

$$\boxed{\zeta_{loc} = A_1 \cdot B_1 \cdot C_1} \quad ([1] \text{ diagram 6.1})$$

Darcy friction factor:

$$\boxed{\lambda = f \left(\text{Re}, \frac{\Delta}{D_h} \right)}$$

See [Straight Pipe - Circular Cross-Section and Nonuniform Roughness Walls \(IDELCHIK\)](#)



Pressure loss friction factor:

$$\zeta_{fr} = 0.0175 \cdot \delta \cdot \lambda \cdot \frac{R_0}{D_h}$$

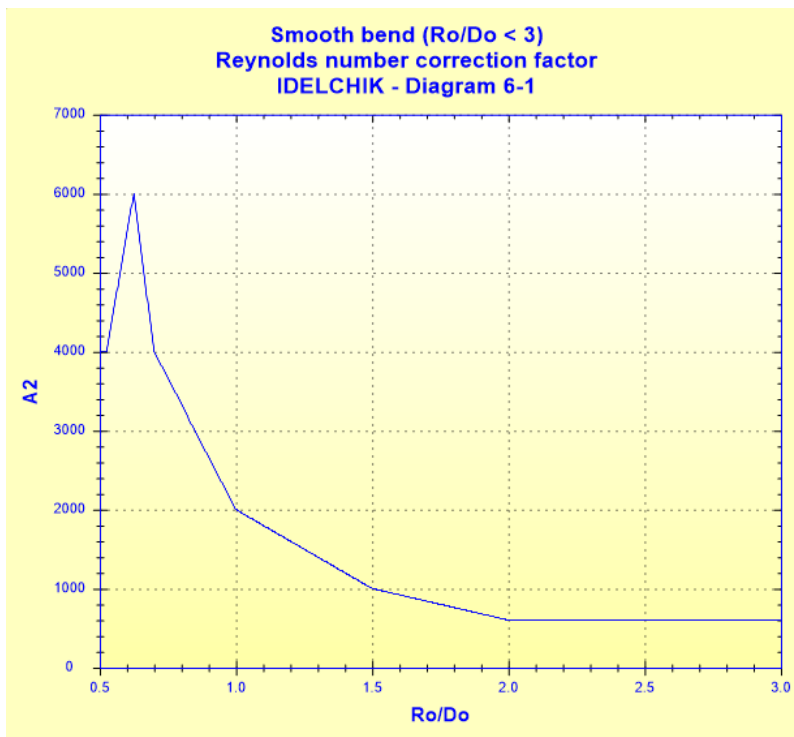
([1] diagram 6.1)

Reynolds number correction factor that depends on the relative curvature radius:

$$A2 = f\left(\frac{R_0}{D_0}\right)$$

([1] diagram 6.1)

R_0/D_0	0.50 - 0.55	>0.55 - 0.70	>0.70 - 1.0	>1.0 - 2.0	>2.0
$A2 \times 10^{-3}$	4.0	6.0	4.0 - 2.0	1.0	0.6



Total pressure loss coefficient:

- $Re \geq 10^4$

$$\zeta = k_{\Delta} \cdot k_{Re} \cdot \zeta_{loc} + \zeta_{fr} \quad ([1] \text{ diagram 6.1})$$

- $3 \cdot 10^3 < Re < 10^4$

$$\zeta = \frac{A_2}{Re} + \zeta_{loc} + \zeta_{fr} \quad ([1] \text{ diagram 6.1})$$

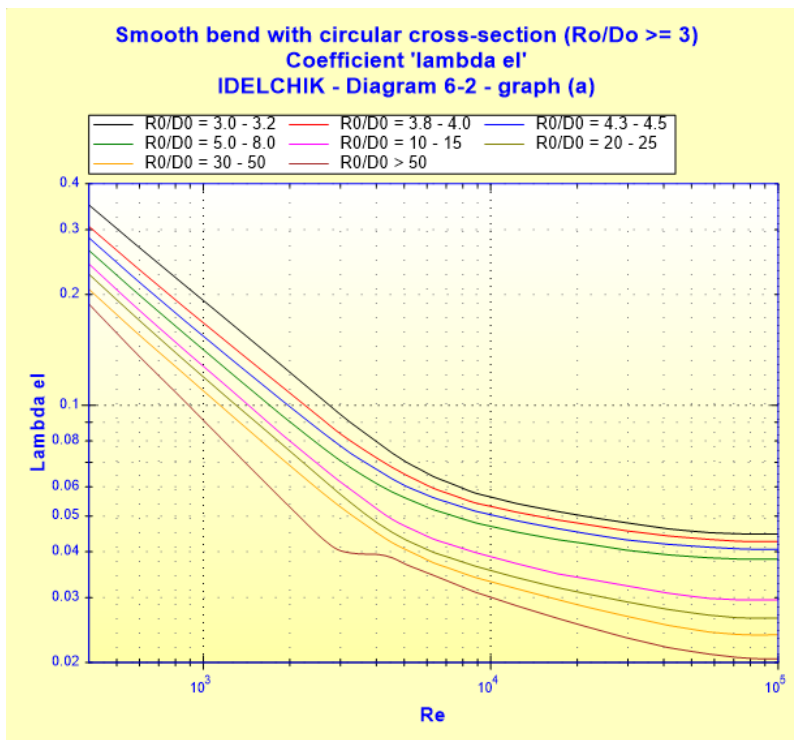
Straight length of equivalent pressure loss (m):

$$L_{eq} = \zeta \cdot \frac{D_0}{\lambda}$$

- Case of relative radius of curvature greater than or equal to 3 ($R_0/D_0 \geq 3$) ([1] diagram 6.2)

Friction factor smooth wall:

$$\lambda_{el} = f\left(Re, \frac{R_0}{D_0}\right) \quad ([1] \text{ diagram 6.2})$$



Roughness correction factor:

$$C_f = \frac{\lambda_r}{\lambda_s} \quad ([2] \text{ equation 9.3})$$

with:

λ_r : Darcy friction factor for rough pipe ($\bar{\Delta} = \Delta/D_h$) at Re

λ_s : Darcy friction factor for hydraulically smooth pipe ($\bar{\Delta} = 0$) at Re

Pressure loss coefficient:

$$\zeta = 0.0175 \cdot \delta \cdot \lambda_{el} \cdot C_f \cdot \frac{R_0}{D_h} \quad ([1] \text{ diagram 6.2 \& [2] equation 9.3})$$

Straight length of equivalent pressure loss (m):

$$L_{eq} = \zeta \cdot \frac{D_0}{\lambda_{el}}$$

Total pressure loss (Pa):

$$\Delta P = \zeta \cdot \frac{\rho \cdot W_0^2}{2} \quad ([1] \text{ diagram 6.1 - 6.2})$$

Total head loss of fluid (m):

$$\Delta H = \zeta \cdot \frac{W_0^2}{2 \cdot g}$$

Hydraulic power loss (W):

$$Wh = \Delta P \cdot Q$$

Symbols, Definitions, SI Units:

D_h	Bend hydraulic diameter (m)
D_0	Bend internal diameter (m)
F_0	Cross-sectional area (m ²)
l	Length measured along the axis (m)
R_0	Radius of curvature (m)
δ	Curvature angle (°)
Q	Volume flow rate (m ³ /s)
w_0	Mean velocity (m/s)
G	Mass flow rate (kg/s)
V	Fluid volume (m ³)
M	Fluid mass (kg)
Re	Reynolds number ()
Δ	Absolute roughness of walls (m)
$\bar{\Delta}$	Relative roughness of walls ()
k_{Δ}	Coefficient that allows for the effect of the roughness
k_{Re}	Coefficient that allows for the effect of the Reynolds number
A_1	Coefficient that allows for the effect of the angle
B_1	Coefficient that allows for the effect of the relative curvature radius
C_1	Coefficient that allows for the effect of the relative elongation of the cross section
ζ_{loc}	Coefficient of local resistance ()
λ	Darcy friction coefficient ()
ζ_{fr}	Pressure loss friction factor ()
ζ	Total pressure loss coefficient (based on the mean velocity in the bend) ()
L_{eq}	Straight length of equivalent pressure loss (m)
λ_{el}	Friction coefficient ()
C_f	Roughness correction factor ()
ΔP	Total pressure loss (Pa)
ΔH	Total head loss of fluid (m)
Wh	Hydraulic power loss (W)
ρ	Fluid density (kg/m ³)
ν	Fluid kinematic viscosity (m ² /s)
g	Gravitational acceleration (m/s ²)

Validity range:

- stabilized flow upstream bend
- length of the straight section downstream: $\geq 10 D_0$
- curvature angle: 0 to 180°
- case of relative radius of curvature lower than 3 ($R_0/D_0 < 3$)
 - flow regime: $Re \geq 3 \cdot 10^3$
- case of relative radius of curvature greater than or equal to 3 ($R_0/D_0 \geq 3$)

- flow regime: $400 \leq Re \leq 10^5$

for Reynolds number 'Re' lower than 400 or greater than 10^5 , the coefficient ' λ_{el} ' is linearly extrapolated.

Example of application:

The screenshot shows the HydraulCalc 2018b software interface. The main window is titled "HydraulCalc 2018b - [Smooth bend with circular cross-section - IDELCHIK (3rd Ed.)]". The interface is divided into several sections:

- Fluid characteristics:**
 - Fluid: Water @ 1 atm [HC]
 - Ref.: IAPWS IF97
 - Temperature: T = 20 °C
 - Pressure: P = 1.013 bar
 - Density: $\rho = 998.2061 \text{ kg/m}^3$
 - Dynamic Viscosity: $\mu = 0.00100159 \text{ N.s/m}^2$
 - Kinematic Viscosity: $\nu = 1.00340E-06 \text{ m}^2/\text{s}$
 - Graph: Density (kg/m³) vs Temperature (°C) showing a decreasing trend from 1000 at 10°C to approximately 950 at 100°C.
- Geometrical characteristics:**
 - Diagram of a 90-degree bend with a circular cross-section.
 - Hydraulic diameter: $D_0 = 0.0703 \text{ m}$
 - Relative radius of curvature: $R_0 = 0.175 \text{ m}$
 - Relative roughness: $\Delta = 1.0E-05 \text{ m}$
 - Flow rate: $G = 4.9910 \text{ kg/s}$, $Q = 0.005 \text{ m}^3/\text{s}$
 - Mean velocity: $w_0 = 1.288 \text{ m/s}$ (Turbulent)
 - Pressure loss: $\Delta P = 0.002119318 \text{ bar}$, $\Delta H = 0.0216 \text{ m of fluid}$
- Complementary results:**

Designation	Symbol	Value	Unit
Hydraulic diameter	D_h	0.0703	m
Cross-sectional area	F_0	0.003881508	m ²
Relative radius of curvature	R_0/D_0	2.489331	
Developed straight length from the axis	l	0.2748893	m
Internal bend volume	V	0.001066985	m ³
Internal bend volume	M	1.065071	kg
Relative roughness	Δ	0.0001422475	
Reynolds number	Re	90251	
Coefficient of local resistance	ζ_{loc}	0.1337544	
Roughness correction (Diagram 6-1)	k_{λ}	1.010951	
Reynolds number correction factor (Diagram 6-1)	k_{Re}	1.340831	
Darcy Friction Factor	λ	0.01907611	
Coefficient of friction resistance	ζ_{fr}	0.07459201	
Pressure loss coefficient (based on the mean bend velocity)	ζ	0.2558981	
Hydraulic power loss	W_h	1.059659	W
Straight length of equivalent pressure loss	Leq	0.9430454	m

References:

- [1] Handbook of Hydraulic Resistance, 3rd Edition, I.E. Idelchik
- [2] Internal Flow System, Second Edition, D.S. Miller